# Supplying Synthetic Crude Oil from Canadian Oil Sands: A Comparative Study of the Costs and CO2 Emissions of Mining and In-Situ Recovery

Aurélie Méjean and Chris Hope

March 2010

CWPE 1014 & EPRG 1005



# Supplying Synthetic Crude Oil from Canadian Oil Sands: A Comparative Study of the Costs and CO<sub>2</sub> Emissions of Mining and In-situ Recovery

EPRG Working Paper 1005 Cambridge Working Paper in Economics 1014

# Aurélie Méjean and Chris Hope

#### Abstract

High crude oil prices and the eventual decline of conventional oil production raise the issue of alternative fuels such as non-conventional oil. The paper describes a simple probabilistic model of the costs of synthetic crude oil (SCO) produced from Canadian oil sands. Synthetic crude oil is obtained by upgrading bitumen that is first produced through mining or in-situ recovery techniques. This forward-looking analysis quantifies the effects of learning and production constraints on the costs of supplying synthetic crude oil from Canadian bitumen deposits. The results show the uncertainties associated with the future costs of synthetic crude oil. Carbon costs have a large impact of the total costs of synthetic crude oil, in particular in the case of synthetic crude oil from in-situ bitumen, due to the carbon-intensity of the recovery techniques. The influence of each parameter on the supply costs is examined. In the case of mined SCO, the maximum production rate, the ultimate recovery rate and the depletion parameters show the largest influence on the results, while learning parameters dominate in the case of in-situ SCO.

#### **Keywords**

Non-conventional oil; Uncertainty; Social cost of carbon

Contact Publication Financial Support a.mejean@jbs.cam.ac.uk March 2010, Revised June 2010 ESRC, TSEC 2



www.eprg.group.cam.ac.uk



# **Electricity Policy Research Group**

**JEL Classification** 

Q42, Q47, Q54



# Supplying synthetic crude oil from Canadian oil sands: a comparative study of the costs and CO<sub>2</sub> emissions of mining and in-situ recovery

Aurélie Méjean<sup>1</sup>

**Chris Hope** 

3<sup>rd</sup> March 2010, Revised 15<sup>th</sup> June 2010

### 1. Introduction

There are growing concerns about whether a petroleum-based economy can be sustained in the coming decades (Greene et al., 2005). High crude oil prices, uncertainties about the consequences of climate change and the eventual depletion of conventional oil resources raise the issue of alternative fuels, such as non-conventional oil. In particular, bitumen can be extracted and upgraded into synthetic crude oil, a substitute to conventional oil (AEUB, 2006).

Climate change is a "serious and urgent issue" (Stern, 2007). Anthropogenic  $CO_2$  emissions accumulate in the atmosphere, leading to enhanced greenhouse effects and climate change. There are large uncertainties associated with this issue, from the scale of the impacts of climate change to the costs of mitigation (Stern, 2007 p33), but there is a growing consensus that this is an issue that the oil industry cannot ignore (Browne, 2006). Climate change analysts have traditionally focused on the aggregate carbon content of global fossil energy resources to argue that the extended use of fossil fuels is not compatible with atmospheric stabilisation targets for  $CO_2$ . However, the distribution of resources across the different fossil fuels also matters, as even a 450ppm target for  $CO_2$  concentrations would allow total carbon emissions over this century to be substantially larger than those which would be produced by burning the total estimated resource base of conventional oil and gas. According to Grubb (2001), "the longer-term problem of climate change arises from the fuller and longer-term use of coal, and of unconventional deposits such as heavy oils, tar sands and

<sup>&</sup>lt;sup>1</sup> Corresponding Author – *E-mail address*: a.mejean@jbs.cam.ac.uk

The authors acknowledge the financial support of the ESRC Electricity Policy Research Group (EPRG). The authors also wish to thank the members of the Electricity Policy Research Group and an anonymous reviewer for their constructive comments.

oil shales." As conventional oil becomes scarcer, the transport sector will remain dependent on petroleum resources, if no oil substitute is available. Fuels from non-conventional oil resources are therefore likely to become the 'backstop fuel'. However, these resources involve higher  $CO_2$  emissions per unit of energy produced than conventional oil and gas, as they require more energy to be extracted and upgraded (Grubb, 2001). In terms of investments in energy technologies, oil companies are expected to push towards 'the frontier of petroleum exploitation' rather than towards the renewable frontier (Grubb, 2001).

The role of technological change and learning has been well studied for lowcarbon and other energy technologies (see for instance Grübler et al., 1999 and McDonald and Schrattenholzer, 2001). As is the case for most emerging technologies, the cost reduction resulting from experience or cumulative production is an argument in favour of investing in new, less carbon intensive energy technologies. The role of learning-by-doing in driving down costs has not normally been taken into account for non-conventional oil in climate change modelling, and Odell (1999) recommends that this inherent contradiction should be eliminated in order to "build an internally consistent model for the evolution of the global energy market".

This paper describes a simple probabilistic model for projecting the cost of supplying bitumen from mining and in-situ recovery methods, and the cost of supplying synthetic crude oil upgraded from mined and in-situ bitumen. The impact of the social cost of  $CO_2$  on the costs of producing these fuels is also assessed. The model uses uncertain parameters, and Monte-Carlo simulations are performed to obtain the probability distribution over time of the costs of synthetic crude oil, with and without the social cost of carbon.

# • 2. Theoretical framework and literature review

This analysis aims to inform decision-making by assessing the future costs of supplying synthetic crude oil and the associated uncertainties. In particular, the influence of learning and depletion on these costs is examined.

# 2.1 Decision theory, uncertainty and subjective probabilities

Decision theory is "designed to help a decision maker choose among a set of alternatives in light of their possible consequences"; each alternative is associated with one or more probability distributions (Web Dictionary of Cybernetics and Systems, 2007). One approach to measure the uncertainty of events is to use subjective probabilities that are based on reasonable assessments by experts. Bayesian theory uses these probabilities to represent the degree of belief of a subject.

The aim here is to express our uncertainty about the future costs of supplying alternative fuels. Uncertainty about future energy prices and technological developments is at the core of the economics of climate change, as the pace of technological change will greatly influence the costs of mitigating greenhouse gas emissions. Numerical modelling is used as a tool to help decision-making: a model is introduced that draws on the user's degree of belief about a series of parameters as an input (for example, Hope, 2006). A probability distribution is assigned to these parameters and the basis of these probabilities is "up-to-date knowledge from science and economics" (Stern, 2007 p33). The uncertainty associated with the validity of the input data is looked at, together with the influence of each parameter on the output.

According to Tversky and Kahneman, the subjective assessment of probability is often based on three heuristics: representativeness, availability and anchoring (1974, p3), which in turn lead to predictable biases. In particular in the case of anchoring, a bias is introduced by subjects who choose a single value as a starting point to assess a probability distribution. Tversky, Kahneman and other authors (Alpert and Raiffa 1969, Staël von Holstein 1971, Winkler 1967, as cited in Tversky and Kahneman 1974) note that these distributions show "large and systematic departures from proper calibration". This is explained by the fact that "subjects state overly narrow confidence intervals which reflect more certainty than is justified by their knowledge about the assessed quantities" (Tversty and Kahneman, 1974 p17).

The tendency to underestimate the uncertainty associated with probability distributions should be avoided. Therefore the distributions assigned to the input parameters of the model will be assessed using as large number of sources and estimates as possible. This justifies the wide ranges that were chosen in this study.

## 2.2 Learning

Learning curves have been used in several areas to identify technologies that could become competitive with adequate investment (Grübler et al., 1999). To build a consistent model for energy supply, technological change should be taken into account for non-conventional oil as well as for renewable energy technologies.

Experience curves are a powerful tool for energy policy making, they are used to "assess the prospects for future improvements in the performance of a technology" (IEA, 2000). They give an indication of the investments that are needed to make a technology competitive (IEA, 2000). Experience curves are normally described by the mathematical expression<sup>2</sup> shown in equation 1.

<sup>&</sup>lt;sup>2</sup> The costs presented here are marginal costs, i.e. the sum of marginal capital costs and marginal operating costs.

$$C_{t} = C_{0} \cdot \left(\frac{X_{t}}{X_{0}}\right)^{-b}$$

$$C_{t} \text{ is the unit cost at time } t$$

$$C_{t} \text{ is the initial unit cost}$$

$$(1)$$

 $C_0$  is the initial unit cost  $X_t$  is the cumulative production at time t  $X_0$  is the initial cumulative production t is the time b is the experience curve parameter or learning coefficient (no unit),  $b \ge 0$ .

Parameter *b* characterises the curvature of the experience curve. The learning rate (*LR*) is a parameter that expresses the rate at which costs decrease each time cumulative production doubles, and is given by:  $LR = 1 - 2^{-b}$ . Cost reductions are ultimately limited by physical constraints, and a 'bottom line cost' (Tsuchiya and Kobayashi, 2003) should be introduced to generalise the relationship, as shown in (Anderson and Winne, 2003):

$$C_{t} = C_{\min} + (C_{0} - C_{\min}) \cdot \left(\frac{X_{t}}{X_{0}}\right)^{b}$$
(2)

 $C_{min}$  is the minimum unit cost

#### **2.3 Depletion**

Depletion should also be taken into account when assessing the prospects for the costs of supplying fossil fuels. The simplest model assumes that the costs of extracting the resources are constant and independent of the remaining stock and of the extraction rate (Hotelling, 1931). Alternative models assume increasing marginal extraction costs as the resource is depleted or increasing marginal extraction costs with the extraction rate, or both (Sweeney, 1992 p13).

Krautkraemer and Toman argue the basic constant extraction cost model wrongly assumes fixed and homogeneous resources and no change in extraction technology<sup>3</sup> (2003 p6). Non-renewable energy resources are in fact heterogeneous, as their quality and difficulty of extraction vary within and among deposits. They suggest incorporating the remaining stock of resources in the extraction cost function as a way to account for resource heterogeneity (Krautkraemer and Toman, 2003 p7).

Oil extraction costs are dependent upon the quality of the resource, and Sweeney shows that low-cost, high-quality resources will be produced before high-cost, low-quality resources: under competition, it is economically rational to produce the low cost, high quality resources first. It follows that under a given state of knowledge, the oil industry shows increasing costs, as an increase in output

<sup>&</sup>lt;sup>3</sup> In this section we assume no technological change in extraction technologies. The learning effect will be treated separately.

means that more is produced from high cost, low quality resources (Adelman, 1993 p9).

The approach taken by modellers is to try to reflect how costs could evolve with the growing difficulty of obtaining the resources under a given state of knowledge. In the RICE-99 model, Nordhaus and Boyer (1999) introduced a carbon-energy supply curve with carbon fuels available at rising costs. Chakravorty and Roumasset have also shown that a rising and convex extraction cost function predominates in the oil industry (1990).

Both depletion and technological advances are driving the supply of exhaustible energy resources and both need to be taken into account to forecast future nonconventional oil extraction costs. The combination of both effects results in a Ushaped cost curve for non-conventional oil.

# 2.4 Non-conventional oil

Conventional and non-conventional oil are usually distinguished by their physical properties: viscosity and density. Viscosity is a measure of the fluid's resistance to flow. It varies greatly with temperature. The oil viscosity at reservoir temperature determines how easily oil flows to the well for extraction. Oil density is a measure of mass per unit volume it is expressed in degrees of API gravity (USGS, 2003).

Conventional oil (also called light oil) has an API gravity  $\ge 22^{\circ}$  and a viscosity < 100 centipoises (cP). Medium-heavy oil is an asphaltic, dense (low API gravity) and viscous oil with 18°API<Density<25°API and 10cP<Viscosity<100cP. It is mobile at reservoir conditions.

Extra-heavy oil is more viscous and dense than medium-heavy oil (density<20°API and 100cP<viscosity<10,000cP). It is still mobile at reservoir conditions. Bitumen is a bit more dense oil and more viscous than extra-heavy oil (density<12°API and 10,000cP<viscosity). It is not mobile at reservoir conditions (Cupcic, 2003).

Conventional oil can also be defined as oil produced by primary or secondary recovery methods (own pressure, physical lift, water flood, and water or natural gas pressure maintenance), while non-conventional oil is not recoverable in its natural state through a well by ordinary oil production methods (Grand Dictionnaire Terminologique, 2007). Bitumen does not flow at reservoir conditions and usually occurs in oil sands. When near the surface, oil sands are excavated and bitumen is extracted from the mined material. When the resource is at greater depth, bitumen is recovered in-situ. Steam and solvents are injected into the reservoir to make the bitumen mobile so that it flows to the surface (Alberta EUB, 2005). Crude bitumen extracted from oil sands is upgraded into synthetic crude oil through carbon removal and hydrogen addition. Synthetic crude oil has similar characteristics as conventional crude oil, and can be refined.

#### 3. Research design

#### 3.1 Methodology

#### a) Model - Learning and depletion

Equation 3 summarises the first version of the supply cost model for bitumen, including learning and depletion effects as it was introduced in (Méjean and Hope, 2008).

$$C_{Bitumen,t} = C_{\min} + (C_{Bitumen,0} - C_{\min}) \cdot \left(\frac{X_{Bitumen,t}}{X_{Bitumen,0}}\right)^{-b} + C_{\max} \cdot \left(\frac{X_{Bitumen,t}}{X_{T}}\right)^{\gamma}$$
learning depletion (3)

 $X_{Bitumen,t}$  is the cumulative production at time t  $C_{Bitumen,t}$  is the cost of bitumen at time t  $X_{Bitumen,0}$  is the initial cumulative production  $C_{Blitumen,0}$  is the initial cost  $C_{min}$  is the minimum cost of producing the resources b is the learning coefficient R is the recovery factor Q is the total oil in place  $C_{max}$  is the maximum cost of the depletion  $\gamma$  is the exponent of the depletion curve  $X_T$  is the ultimately recoverable resources,  $X_T = Q^*R$ 

Learning and depletion are driven by production  $(X_t)$ . Learning drives costs down, and depletion drives costs up, as the resources become depleted and become more difficult to extract.  $X_T$  is obtained by multiplying two parameters: the total oil in place (*Q*) and the recovery factor (*R*). The learning coefficient *b* defines the pace at which technological change is driving costs down, and the exponent of the depletion cost curve gamma defines the pace at which depletion is driving costs up. The cumulative production at time t ( $X_t$ ) is exogenous. The exponential form of the depletion part of the cost function is flexible as its parameters can be changed to fit simple as well as more sophisticated models.

#### b) Production

The cumulative production at time t (X<sub>t</sub>) is obtained by summing over time the production rate at time t ( $x_t$ ). The production rate is assumed to follow an S-curve: it grows exponentially before reaching a plateau (see Soderbergh, 2006). The production rate is modelled as shown in equation 4.

$$x_{t} = \frac{a}{c + e^{-d \cdot t}}$$
(4)
$$x_{t} \text{ is the production rate (barrels/year)}$$

 $\frac{a}{c}$  is the maximum production rate (barrels/year)

 $t_1$  is the inflection point, which determines d

Parameters *a* and *c* are defined by the upper bound of production capacity when time tends towards infinity and the actual production at time 0.

$$\lim_{t \to \infty} x_t = \frac{a}{c} \quad ; \quad x_0 = x_{t=2005}$$

This model is not entirely satisfactory, as the production rate is determined exogenously. In practice, the production rate will depend on conventional and non-conventional oil prices, which will be influenced by the cost of producing oil and should be decreasing in the longer-term because of depletion.

c) The social cost of carbon

The social cost of  $CO_2$  is the increase in future damage, discounted to the present day, that occurs if current emissions of  $CO_2$  are increased by one ton. The social cost of  $CO_2$  is increasing with time at the rate  $\alpha$ , to account for the increasing damage costs over time:

$$C_{CO_2,t} = C_{CO_2,0} \cdot e^{\alpha(t-t_0)}$$
<sup>(5)</sup>

 $C_{CO2,t}$  is the social cost of emitting CO<sub>2</sub> at time t (USD/tCO<sub>2</sub>)  $C_{CO2,0}$  is the social cost of emitting CO<sub>2</sub> at time 0 (USD/tCO<sub>2</sub>)  $\alpha$  is the rate of increase of the social cost of carbon with time t

The specific costs of carbon from bitumen production are calculated from the process unit emissions e as follows:

$$C_{Bitumen,t}^{CO_2} = C_{CO_2,t} \cdot e_{Bitumen,t}$$
(6)

 $C_{Bitumen,t}^{CO_2}$  is the carbon cost associated with the production of bitumen (USD/barrel)

 $C_{CO2,t}$  is the social cost of emitting CO<sub>2</sub> at time t (USD/tCO<sub>2</sub>)

 $e_{Bitumen,t}$  is the CO<sub>2</sub> emissions to produce one barrel of bitumen (tCO<sub>2</sub>/barrel)

Unit emissions are assumed to decline with cumulative emissions because of greater efficiency in the extraction process.

$$\boldsymbol{e}_{Bitumen,t} = \boldsymbol{e}_{\min} + (\boldsymbol{e}_{Bitumen,0} - \boldsymbol{e}_{\min}) \cdot \left(\frac{\boldsymbol{E}_{Bitumen,t}}{\boldsymbol{E}_{Bitumen,0}}\right)^{-b_e}$$
(7)

 $e_{Bitumen,t}$  is the CO<sub>2</sub> emissions to produce bitumen at t (tCO<sub>2</sub>/barrel)  $e_{Bitumen,0}$  is the CO<sub>2</sub> emissions to produce bitumen at time 0 (tCO<sub>2</sub>/barrel)  $E_{Bitumen,t}$  is the cumulative CO<sub>2</sub> emissions from bitumen production at t (tCO<sub>2</sub>)

 $E_{Bitumen,0}$  is the cumulative CO<sub>2</sub> emissions from bitumen production at time 0 (tCO<sub>2</sub>)

 $e_{min}$  is the minimum CO<sub>2</sub> emissions to produce bitumen (tCO<sub>2</sub>/barrel)  $b_e$  is the learning coefficient

The same equations apply to the carbon costs and emissions associated with upgrading bitumen into synthetic crude oil.

#### d) Upgrading bitumen into synthetic crude oil

Upgrading is the process to convert mined bitumen and bitumen produced insitu into synthetic crude oil. Synthetic crude oil (SCO) has similar density and viscosity to conventional light-medium crude oil (AEUB, 2003). Bitumen is upgraded into synthetic crude oil by adding hydrogen, subtracting carbon, or both (AEUB, 2003). In our model, upgrading costs are decreasing with cumulative upgrading capacity.

$$C_{Upgrading,t} = C_{Upgrading,\min} + (C_{Upgrading,0} - C_{Upgrading,\min}) \cdot \left(\frac{X_{Upgrading,t}}{X_{Upgrading,0}}\right)^{-b_U}$$

 $C_{Upgrading,t}$  is the cost of upgrading bitumen into SCO (USD/barrel SCO)  $C_{Upgrading,min}$  is the minimum cost of upgrading bitumen(USD/barrel SCO)  $X_{Upgrading,t}$  is the cumulative upgrading capacity (barrels SCO)  $X_{Upgrading,0}$  is the cumulative upgrading capacity at time 0 (barrels SCO)  $b_U$  is the learning coefficient (no unit)

#### e) Supply costs of synthetic crude oil

The costs of supplying synthetic crude oil are calculated as follows:

$$C_{\text{SCO},t} = \frac{C_{\text{Bitumen},t}}{k} + C_{\text{Upgrading},t}$$
(9)

*k* is the conversion efficiency from bitumen to synthetic crude oil (barrels SCO per barrel bitumen)

When taking into account  $CO_2$  emissions and costs, the equation for total synthetic crude oil costs becomes:

$$C_{\text{SCO},t} = \frac{C_{\text{Bitumen},t} + C_{\text{Bitumen},t}^{\text{CO}_2}}{k} + C_{\text{Upgrading},t} + C_{\text{Upgrading},t}^{\text{CO}_2}$$
(10)

The learning, depletion and production parameters described above are not known precisely. The effect of uncertainty associated with these input variables on the resulting supply costs should be explored: uncertainty is introduced in the model by assigning subjective probability distributions to the model parameters.

## 3.2 Parameters for Canadian bitumen

A triangular distribution is assigned to each parameter. Each distribution is defined by a minimum, a maximum and a most likely value. The direction of the skew of the triangular distribution is set by the size of the most likely value relative to the minimum and the maximum (Palisade, 2007). A literature review is conducted in order to define the ranges of estimates associated with each parameter.

#### a) Production parameters

# Maximum production rate $(x_{max})$ , initial production rate $(x_0)$ and inflection time $(t_1)$

The range of production rate estimates found in the literature are summarized on Figures 1 and 2 for mined and in-situ produced bitumen, respectively.



Fig. 1: Literature estimates for the production rate over time - mined bitumen



Fig. 2: Literature estimates for the production rate over time - in-situ bitumen

The ranges in table 1 are assigned to production parameters  $t_1$  (inflection time),  $x_0$  (initial production rate) and  $x_{max}$  (maximum production rate) to cover the literature estimates in figures 1 and 2. Triangular distributions are assigned to the production parameters and the most likely values shown in table 1 correspond to the model mean shown in figures 1 and 2.

	MINING			IN-SITU		
MINING	Min	Most likely	Max	Min	Most likely	Max
t <sub>1</sub> , year	2009	2012	2015	2010	2013	2014
x <sub>0</sub> , barrels per day	6.0E+05	7.5E+05	9.0E+05	2.0E+05	4.0E+05	6.0E+05
x <sub>max</sub> , barrels per	1.6E+06	2.4E+06	3.1E+06	1.6E+06	2.65E+06	3.7E+06

Table 1: Production parameters estimates

#### Initial cumulative production (X<sub>0</sub>)

The initial cumulative production of bitumen from mining and in-situ recovery techniques was obtained using historical data from (CAPP, 2009) (cf. Appendix). The initial cumulative production of mined bitumen is 3.2E+09 barrels (1967 – 2005) while the initial cumulative production of bitumen from in-situ recovery techniques is 1.6E+09 barrels (1967 – 2005). In this study, we will assume that all mined and in-situ produced bitumen is upgraded to SCO.

#### b) Resource parameters

#### *Ultimate volume in place (Q)*

A distinction must be made between the amount of bitumen physically occurring underground, and the amount of bitumen that will eventually be recovered from the deposits. We define the amount of bitumen physically occurring underground before any extraction has taken place as the ultimate volume in place. The ultimate volume of bitumen in place in Canada is estimated at about 2.5 trillion barrels (NEB, 2004 p4). Of the 2.5 trillion barrels of bitumen in place, about 0.14 trillion barrels would be "amenable to surface mining" (with an overburden thickness of 75 metres or less), while about 2.4 trillion barrels would be recoverable using in-situ production technologies (NEB, 2004 p4). The ranges of the ultimate volume in place are constructed around these estimates, with a 10% uncertainty range (see table 2).

Ultimate	volume	in	place,	Minimum	Most likely	Maximum
MINING				0.13E+12	0.14E+12	0.15E+12
IN-SITU				2.16E+12	2.40E+12	2.64E+12
				-	-	

Table 2: Ultimate volume in place estimates

#### Recovery factor (R)

The recovery factor is the percentage of the total oil in place in a deposit that can be recovered by a combination of primary, secondary and tertiary techniques (Grand Dictionnaire Terminologique, 2007). In our study, the ultimate recovery factor is the amount of oil or bitumen that could ultimately be produced as a percentage of the total amount of bitumen in place.

According to the AEUB (2003 p2-8), the ultimate recoverable bitumen resources using surface mining techniques are estimated at about  $1E+10m^3$ , i.e. 0.063E+12 barrels, or about 42% of the ultimate volume in place (mining). The estimated recovery factor for surface coal mining is 0.8 to 0.9, (USGS, 1989). The range for the mining recovery factor is thus chosen as 0.42 - 0.9.

According to the AEUB (2003 p2-8), the ultimate recoverable bitumen resources using in-situ techniques are about 3.9E+10 m<sup>3</sup>, i.e. 0.25E+12 barrels, or about a tenth of the ultimate volume in place (in-situ). The estimates of the recovery factors available in the literature are closely linked to the performance of current technologies, and to current or anticipated economic conditions. Ideally this study should be conducted independently of these considerations, as it is very difficult to anticipate future technological breakthroughs and economic conditions. In Rogner's hydrocarbon resource assessment, "the broadest possible dimensions were applied without immediate reference to recoverability" (1997 p220). Rogner points out the "difficulty of incorporating future development efforts, technology change, and uncertainty into reserve assessments" and argues for the inclusion of all hydrocarbon occurrences, as the "a priori exclusion of presently subeconomic or geologically uncertain occurrences would certainly

underestimate the hydrocarbon occurrence potentially available to humankind", (1997 p236). Rogner thus adopts the highest plausible value for the occurrences of non-conventional oil resources, as his objective is to assess "the ultimately available resource base beyond short-term techno-economic recovery limitations" (1997 p253).

Our model introduces a depletion cost component that is solely based on the growing physical difficulty of producing bitumen. The recovery factor used to determine the costs associated with the depletion of the resources should therefore be set at the highest possible value. The previous estimates of the recovery factor are considered to be conservative, they will be chosen as the lower bound of the ranges. Table 3 shows the final estimates of the recovery rate used in the model.

Recovery factor, no unit	Min	Most likely	Max
MINING	0.42	0.71	0.9
IN-SITU	0.11	0.56	0.6

Table 3: Recovery factor estimates

#### c) Depletion parameters

#### Maximum costs ( $C_{max}$ ) and depletion exponent ( $\gamma$ )

The estimates of the depletion parameters are obtained using the method described in (Méjean and Hope, 2008). Estimates from Attanasi (used in the SAUNER project), Rogner and Nordhaus and Boyer are used to determine the depletion parameters' ranges. The incremental cost function from which some of these estimates are derived expresses "the quantity of resources that the industry is capable of adding to proved reserves or cumulative production" as a function of long-term marginal costs (Attanasi, 1995, p2). These curves assume no subsequent cost reductions through technology learning (IEA, 2005a). The European SAUNER project uses Attanasi's estimates to produce world oil supply cost curves for various categories of oil, including tar sands. Rogner (1997) also produced similar aggregate quantity–cost curves for global oil resources. The resulting estimates for  $\gamma$  and C<sub>max</sub> are summarised in table 4.

	SAUNER 2000	SAUNER 2000	Rogner 1997 p254	Nordhaus and Boyer 1999 p40
Category	Tar sands	Conventional oil	Global oil resources	Carbon fuels
γ (no unit)	1.07		1.04	4
<i>Cmax</i> (2005)USD/barrel	186*	120	240**	121***

\*155 (1998)USD; \*\*160 (1990)USD; \*\*\*81 (1990)USD

Table 4: Literature estimates for depletion parameters

Rogner values all resource categories are as if "all future productivity gains were realized immediately" (p253). In his analysis, "a productivity gain in the upstream sector of 1% per year is assumed (...) a resource that presently commands production costs of, for example, \$40 per barrel of oil equivalent (boe) would, over a period of 50 years, drop gradually to \$24", (Rogner, 1997 p251). The high end of the conventional oil spectrum is 35 (1990) USD/barrel (including EOR). Taking out the 1% per year productivity gains, this is equivalent to 58 (1990) USD/barrel, or 86 (2005) USD/barrel (Rogner, 1997 p254). The high end of the non-conventional spectrum is 160 (1990) USD/barrel, which is equivalent to 267 (1990) USD/barrel without any productivity gain, or 395 (2005) USD/barrels (Rogner, 1997 p254).

The SAUNER project models production costs in 1998 USD per barrel. The highest conventional oil production costs are 50 (1998) USD/barrel (SAUNER, 2000b), or 60 (2005) USD/barrel. The depletion exponent is chosen between 1 and 4, but the probability distribution is skewed towards the lower bound of the range because a degree convexity corresponding to a value of 4 is considered to be very high in the case of the oil sands as these resources are well known. The maximum depletion cost parameters are chosen as shown in table 5.

Cmax	minimum	maximum
Bitumen	121**	395*
Conventional oil	60***	86*

\*adapted from Rogner, \*\*adapted from Nordhaus and Boyer, \*\*\* adapted from SAUNER

Table 5: Maximum depletion costs ranges used in the model *d*) *Learning parameters* 

#### Initial costs (C<sub>0</sub>)

Table 6 summarises the operating and supply costs of bitumen recovered using cold production, various in-situ techniques and surface mining. Upgrading costs are also included.

USD(2005) per barrel at the plant gate	Output	Operating costs	Supply costs	Source
In-situ (cold production)				
Wabasca, Seal	bitumen	5 - 7	12 - 15	NEB, 2006
Wabaka	bitumen	3.5 – 7.5	8.5 - 12	Cliffe, 2002
CHOPS - Cold Lake	bitumen	7 – 8	13 - 16	NEB, 2006
Cold Lake	bitumen	7 – 11	12 - 16	Cliffe, 2002
In-situ (thermal)	bitumen			
Cyclic Steam Stimulation (CSS)	bitumen	8 - 12	17 - 20	NEB, 2006
CSS	bitumen	7 – 12	12 - 19	Cliffe, 2002
CSS	bitumen	6 - 10	10 - 15	IEA, 2002
CSS	SCO	4.5 - 7.5		NRCan,
Steam Assisted Gravity Drainage (SAGD)	bitumen	8 - 12	15 - 18	NEB, 2006

SAGD	bitumen	6 - 11	10 - 17	Cliffe, 2002
SAGD	bitumen	5 – 9	7 - 13	IEA, 2002
SAGD	SCO	3.5 – 7		NRCan,
Mining				
Mining/Extraction	bitumen	7 – 10	15 - 17	NEB, 2006
Mining	bitumen	6 - 10	12 - 16	Cliffe, 2002
Mining	SCO	11 - 13.5		NRCan,
Integrated Mining/Upgrading	SCO	15 - 18	30 - 33	NEB, 2006
Integrated Mining/Upgrading	SCO	12-15	18 - 22	Cliffe, 2002
Upgrading				
Stand-alone upgrader	SCO	12 - 15	22 - 27	Cliffe, 2002

Source: (Cliffe, 2002) and (IEA, 2002) are adapted from (Greene, 2003); (NEB, 2006) Table 6: Literature estimates for initial costs

The ranges in table 7 are assigned to the initial mining, thermal in-situ and upgrading costs.

C <sub>0</sub> , 2005 USD/barrel	Minimum	Most likely	Maximum
MINING	12	15	17
IN-SITU (thermal)	7	14	20
STANDALONE UPGRADER	22	25	27

Table 7: Initial costs ranges used in the model

It should be noted that the model does not include a parameter that reflects the losses occurring at the extraction stage. Bitumen is extracted from the mined oil sands before it is sent to the upgrader to be transformed into synthetic crude oil. These losses currently come close to about 10 to 13% of the initial amount of bitumen occurring in the mined oil sands (Alberta Chamber of Resources, 2004 p20). These losses have an impact on the bitumen production rate and the unit costs of producing bitumen. In fact, these losses are already included in the model, but in an implicit way. The estimates used to construct the ranges for the initial costs are found in the literature in dollars per barrel of bitumen, not in dollars per barrel of oil sand. These costs therefore already account for the losses occurring at the extraction stage. Similarly, the estimates obtained for future production rates are found in barrels of bitumen, and not in barrels of mined oil sands. Also, the estimation of the minimum mining costs ( $C_{min}$ ) takes these losses into account (see paragraph below).

#### Minimum costs (C<sub>min</sub>)

The minimum costs of mining bitumen were estimated between 2 and 9 USD per barrel of bitumen in (Méjean and Hope, 2008). The minimum costs of producing bitumen through in-situ recovery techniques are estimated by examining the costs of producing Venezuelan heavy oil. Venezuelan heavy oil from the Orinoco belt flows at reservoir temperature and can be produced without additional "viscosity-reduction techniques" (IEA, 2005 p77). Greene (2003 p19) estimates the extraction costs of Venezuelan heavy oil at about 3 USD/barrel, and upgrading costs at over 4 USD/barrel. Also, the costs of primary recovery of heavy oil in difficult offshore areas can be as low as USD2/barrel (Roumasset et al., 1983). The range for the minimum cost of producing bitumen through in-situ recovery is chosen as 2 to 3 USD/barrel.

The upgrading stage integrates mature refinery processes in an original way. The minimum upgrading costs can be estimated using current petroleum refining costs. Several refining cost estimates were found in the literature, for instance refining cost estimates of 7.01 USD/barrel (including marketing and energy costs) (EIA, 2007 p33) and operating costs between 5 and 8 USD/barrel between 1988 and 2001 (EIA, 2003 p6). The ranges in table 8 are assigned to minimum cost estimates.

<i>C<sub>min</sub></i> , USD/barrel (bitumen or SCO)	Minimum	Most likely	Maximum
MINING	2	5.5	9
IN-SITU	2	2.5	3
UPGRADING	4	6.5	8

Table 8: Minimum cost ranges used in the mode
---

#### Learning rate (LR)

Some learning rate estimates for petroleum refining and chemical refining found in the literature are summarized in table 9.

Type of process	Learning	rate	(no	Source
Oil refining	0.1			Emerson, 1988 p138 in (Junius, 1997)
Chemical products	0.2 – 0.3			Lieberman, 1984 p221
Conventional oil technologies	0.04			Kahouli-Brahmi, 2008 p141

Table 9: Literature estimates for the learning rate parameter

According to Kahouli-Brahmi (2008 p 141) "mature technologies such as coal, oil and lignite conventional technologies present relatively low learning rates of 4% on average". The learning rate for Canadian bitumen production was estimated between 0.2 and 0.42 in (Méjean and Hope, 2008). The lower bound of the range was derived from (IEA, 2005 p166), while the upper bound of the range was calculated using historical data of supply costs and production volumes from the Canadian Petroleum Producers Association (CAPP) from 1983 to 1998. The learning rate of 0.42 is very high compared to other energy technologies (see McDonald and Schrattenholzer, 2001). We expand the previous study and differentiate between bitumen mining and in-situ production technologies.

The learning rate for in-situ bitumen is calculated from production data from CAPP (2009) and supply cost data from NRCan in (Alberta Chamber of Resources, 2004 p12). This regression gives a learning rate of 0.21 for in-situ production (R<sup>2</sup>=0.94) between 1985 and 1991. Toman et al. (2008, p33) assume a more conservative learning rate of 0.10 for bitumen production from Canadian oil sands. As mining is now considered as a mature technology the value of 0.1 is chosen as the lower bound of the mining learning rate range. The following ranges are thus chosen for mining and in-situ learning rates. The learning rate of

0.25 for oil extraction (McDonald and Schrattenholzer, 2001 p257) falls into both bitumen production ranges.

LR, no unit	Minimum	Most likely	Maximum
MINING	0.10	0.26	0.42
IN-SITU	0.21	0.30	0.42
UPGRADING	0.04	0.17	0.3

Table 10: Learning rate ranges used in the model

#### e) Carbon costs and emissions

#### Initial carbon costs $C_{c0}$ and growth rate $\alpha$

The following range for the social costs of carbon in 2008 is obtained from PAGE2002 with Stern review assumption:  $25 - 300 (2000) \text{ USD/tCO}_2$  (Hope, 2008 p20). The social cost of carbon is assumed to grow at a rate of about 2 to 3% per year in real terms (Hope, 2008 p19). The social costs of carbon in year 0 (2005) are thus estimated at about 23 to 283 (2000) USD/tCO<sub>2</sub>, i.e. 26 - 322 (2005) USD/tCO<sub>2</sub> (with 1 USD(2000) = 1.138 USD(2005)).

Carbon parameter	Minimum	Most likely	Maximum
C <sub>c,0</sub> USD/tCO <sub>2</sub>	26	174	322
alpha, no unit	0.02	0.025	0.03
		1.	

Table 11: Carbon parameters ranges used in the model

#### Initial unit emissions $(e_0)$

The literature estimates for unit  $CO_2$  emissions for mining recovery, in-situ recovery and upgrading are summarised in table 12.

Type of process	Initial unit emissions tCO <sub>2eq</sub> /barrel	Source		
Mining	0.04	Alberta Chamber of Resources, 2004 p62		
Mining	0.035	LENEF and T.J.McCann & Associates in (Alberta Chamber of Resources, 2004 p62)		
Mining	0.025 - 0.05	Cupcic, 2003 p24		
In-situ	0.06	Alberta Chamber of Resources, 2004 p62		
In-situ	0.081	CAPP, 2004 p30		
In-situ	0.07 – 0.085	LENEF and T.J.McCann & Associates in (Alberta Chamber of Resources, 2004 p62)		
In-situ (SAGD)	0.065 - 0.115	Cupcic, 2003 p24		
Upgrading	0.075 – 0.09	LENEF and T.J.McCann & Associates in (Alberta Chamber of Resources, 2004 p62)		
Upgrading	0.038	Cupcic, 2003 p24		
Light/medium crude	0.022 (0.18tCO <sub>2eq</sub> /m <sup>3</sup> )*	САРР, 2004 р30		

\*1 barrel = 0.12 m<sup>3</sup>

#### Table 12: Literature estimates for unit emissions

Carbon emissions are expected to increase when natural gas is replaced by residues to produce steam for recovery and hydrogen for upgrading. Flint provides some estimates for carbon emissions per barrel of SCO, shown in table 13.

Emissions (tCO <sub>2eq</sub> /barrel SCO)	In-situ (SAGD	) + upgrading	Mining + upgrading		
Process	Natural gas Residue		Natural gas	Residue	
Total recovery only (tCO <sub>2eq</sub> /barrel bitumen)	0.049-0.054	0.077-0.086	0.027- 0.030	0.037-0.041	
Total upgrading only	0.045	0.085	0.045	0.085	

Table 13: Comparison between natural gas and residue fuelled upgrading processes

The ranges in table 14 are assigned to unit emission parameters.

e <sub>0</sub> , tCO <sub>2eq</sub> /barrel	Min	Most likely	Max
MINING (bitumen)	0.025	0.038	0.05
IN-SITU (bitumen)	0.049	0.083	0.115
UPGRADING (SCO)	0.038	0.064	0.09

Table 14: Unit carbon emissions ranges used in the model

#### Initial cumulative emissions (E)

An estimate for initial cumulative carbon emissions is obtained by multiplying the initial cumulative production of bitumen (in barrels) by the range for initial unit emissions (in  $tCO_{2eq}$  per barrel). This method gives the following estimates, which are chosen as the lower bound of the range, as unit carbon emissions are assumed to have decreased over time in the past.

If we assume that only mined bitumen was upgraded to synthetic crude oil, the cumulative volume of bitumen upgraded equals 3.7E+09 barrels between 1967 and 2005, and the cumulative production of synthetic crude oil equals 2.6E+09 over the same period. An estimate for initial cumulative carbon emissions is obtained by multiplying the initial cumulative production of synthetic crude oil (in barrels) by the range for initial unit emissions (in tCO<sub>2eq</sub> per barrel of synthetic crude oil). This method gives the estimates in table 15, which again are chosen as the lower bound of the range, as unit carbon emissions are assumed to have decreased over time in the past.

Туре	of	Initial	cumulative	Initial unit emissions	Initial	cumulative
process		production	ı (barrels)	(tCO <sub>2eq</sub> /barrel)	emissions (tCC	2e)

Mining	3.9E+09	0.025 - 0.05	0.98E+08 - 2.0E+08
In-situ	1.6E+09	0.06 - 0.115	0.96E+08 - 1.8E+08
Upgrading	2.6E+09 (barrels SCO)	0.038 - 0.09 (tCO <sub>2eq</sub> /barrel SCO)	0.99E+08 - 2.3E+08

Table 15: Literature estimates for initial cumulative emissions

Historical unit emissions from (Alberta Chamber of Resources, 2004 p15) are used to find a higher estimate of the initial cumulative emissions. Unit carbon emissions are multiplied with bitumen production rate each year, and aggregated over the whole period. It should be noted that the carbon emissions data from (Alberta Chamber of Resources, 2004 p15) do not differentiate between in-situ or mining recovery. The following estimates are found:  $4.6E+08 \text{ tCO}_{2eq}$  for initial cumulative emissions from mining and  $1.8E+08 \text{ tCO}_{2eq}$  for initial cumulative emissions from in-situ.

Upgrading uses similar processes as those used in conventional oil refining. The cumulative emissions from petroleum refining in Canada from 1990 to 2005 amounted about  $3.1E+08 \text{ tCO}_{2eq}$  (Environment Canada, 2008 p31). The ranges in table 16 are assigned to the cumulative emissions parameters.

E, tCO <sub>2eq</sub>	Minimum	Most likely	Maximum
MINING	0.98E+08	2.8E+08	4.6E+08
IN-SITU	0.96E+08	1.4E+08	1.8E+08
Upgrading	1.0E+08	2.1E+08	3.1E+08

Table 16: Initial cumulative emission ranges use in the model

#### *Minimum carbon emissions (e<sub>min</sub>)*

According to (Flint, 2004 p65), the use of natural gas for bitumen recovery and hydrogen generation is responsible for over half of  $CO_2$  emissions associated to SCO from mined bitumen, and 75% of  $CO_2$  emissions associated to SCO produced from bitumen recovered in-situ. Also, between 8 and 12% of  $CO_2$  emissions associated to SCO can be attributed to the energy use of the upgrader.

We estimate the "bottom line", minimum achievable carbon emissions for mining and in-situ recovery by assuming that only low-carbon energy is used for recovery and hydrogen production. In the case of bitumen recovery, it follows that both recovery energy and purchased power (see Flint, 2004 p20) have zero carbon emissions. These estimates are used as the lower bound of the range.

As upgrading uses similar processes as those used in conventional oil refining, but applied to a heavier feedstock, we chose the current  $CO_2$  intensity of 0.036 t  $tCO_{2eq}$ /barrel of oil input in a conventional petroleum refinery (Chevron, 2008), as the upper bound of range for upgrading minimum emissions. The upper bound of the minimum  $CO_2$  emissions of the mining and in-situ recovery processes are chosen just below the current emissions (associated to the use of natural gas).

e <sub>min</sub> , tCO <sub>2eq</sub> /barrel	Min	Most likely	Max
MINING	0.015	0.020	0.024
IN-SITU	0.005	0.027	0.048
UPGRADING (tCO <sub>2eq</sub> /barrel SCO)	0.005	0.021	0.036

Table 17: Minimum emissions ranges used in the model

# f) Summary

Table 18 summarises the ranges that are assigned to each parameter in the model.

Parameters	Minimum	Most likely	Maximum	Standard	Unit
<b>D</b>				deviation	
Resources	1.2E+11	1 41 E 11	1 55,11	4.000.00	hamola
Mining resources in place $(Q_M)$	1.3E+11	1.41E+11	1.5E+11	4.09E+09	Darreis
Mining recovery rate ( <i>R<sub>M</sub></i> )	0.42	0.66	0.9	0.10	no unit
In-situ resources in place ( <i>Q</i> <sub>IS</sub> )	2.16E+12	2.4E+12	2.64E+12	9.80E+10	barrels
In-situ recovery rate ( <i>R</i> <sub>IS</sub> )	0.11	0.36	0.6	0.10	no unit
Production					
Initial mining production rate $(x_{M,0})$	6.0E+05	7.5E+05	9.0E+5	6.12E+04	barrels per day
Mining inflection time $(t_{M,1})$	2009	2012	2015	1	year
Maximum mining production rate	1.6E+06	2.2E+06	3.5E+06	3.97E+05	barrels per day
Initial in-situ production rate $(x_{IS,0})$	2.0E+05	4.0E+05	6.0E+05	8.16E+04	barrels per day
In-situ inflection time $(t_{IS,1})$	2015	2028	2040	5	year
Maximum in-situ production rate	1.6E+06	2.7E+06	3.7E+06	4.29E+05	barrels per day
Upgrading efficiency (k)	0.81	0.86	0.9	0.02	no unit
Depletion					
Maximum depletion costs ( $C_{max}$ )	121	258	395	56	USD/barrel
Depletion exponent ( $\gamma$ )	1	1.9	4	0.63	no unit
Learning					
Initial mining costs ( $C_{M,0}$ )	12	15	17	1	USD/barrel
Initial in-situ costs (C <sub>IS,0</sub> )	7	14	21	2.9	USD/barrel
Initial upgrading costs ( $C_{U,0}$ )	22	25	27	1.0	USD/barrel
Mining learning rate (LR <sub>M</sub> )	0.10	0.26	0.42	0.07	no unit
In-situ learning rate (LR <sub>IS</sub> )	0.21	0.32	0.42	0.04	no unit
Upgrading learning rate ( <i>LR<sub>U</sub></i> )	0.04	0.17	0.3	0.05	no unit
Minimum mining costs (C <sub>M,min</sub> )	2	5.5	9	1.4	USD/barrel
Minimum in-situ costs (C <sub>IS,min</sub> )	2	2.5	3	0.2	USD/barrel
Minimum upgrading costs ( $C_{U,min}$ )	4	6	8	0.8	USD/barrel SCO
Carbon					
Initial carbon costs ( $C_{C,0}$ )	26	85	322	64	USD/tCO <sub>2eq</sub>
Carbon costs growth rate ( $\alpha$ )	0.02	0.025	0.03	0.00	no unit
In-situ initial emissions ( <i>e<sub>M,0</sub></i> )	0.049	0.038	0.115	0.02	tCO <sub>2eg</sub> /barrel
Mining initial emissions ( <i>e</i> <sub><i>I</i>S,0</sub> )	0.025	0.02	0.05	0.01	tCO <sub>2eq</sub> /barrel
Upgrading initial emissions ( <i>e<sub>U,0</sub></i> )	0.038	0.064	0.09	0.01	tCO <sub>2eq</sub> /barrel SCO
In-situ cumulative emissions $(E_{M,0})$	0.98E+08	2.8E+08	4.6E+08	7.39E+07	tCO <sub>2eq</sub>
Mining cumulative emissions ( <i>E</i> <sub>1S.0</sub> )	0.96E+08	1.4E+08	1.8E+08	1.72E+07	tCO <sub>2eq</sub>
Upgrading cumulative emissions $(E_{11.0})$	1.0E+08	2.1E+08	3.1E+08	4.29E+07	tCO <sub>2eq</sub>
In-situ minimum emissions ( $e_{M,min}$ )	0.015	0.020	0.024	0.002	tCO <sub>2eq</sub> /barrel
Mining minimum emissions ( <i>e</i> <sub>IS,min</sub> )	0.005	0.027	0.048	0.009	tCO <sub>2eq</sub> /barrel
Upgrading minimum emissions ( <i>e</i> <sub>11.min</sub> )	0.005	0.021	0.036	0.006	tCO <sub>2eq</sub> /barrel SCO

The wide ranges translate the large uncertainty on these parameters. These ranges are illustrative: the figures are better than guesses, as the above discussion shows, but they are not the result of a formal elicitation exercise. It is assumed that all these parameters are independent. These ranges are fed into the model to obtain some cost results.

### • 4. Results

### 4.1 Bitumen costs: with and without carbon

a) Bitumen costs over time

Using the model described earlier and the parameter ranges summarised above, the results shown in figure 3 are obtained for the supply costs of Canadian bitumen over time. These results are obtained from a Monte-Carlo simulation of 10,000 runs. Costs are shown in (2005)USD/barrel.



Fig. 3: Mined bitumen costs over time, with and without carbon costs



Fig. 4: In-situ bitumen costs over time, with and without carbon costs

The centre lines represent the trends in mean value. The outer bands are the  $5^{th}$  and  $95^{th}$  percentiles: the narrower the band, the less the uncertainty about the supply and total costs.

This model reveals the kind of uncertainties that need to be dealt with when designing policies. The results show large uncertainties on future costs of bitumen produced from mining and in-situ recovery techniques, with supply costs (without carbon) falling in the range of 10 to 46 USD per barrel in 2030 (2005 USD) for mined bitumen, while in-situ produced bitumen supply costs fall in the range of 4 to 9 USD per barrel (2005 USD). Learning dominates in the case of in-situ bitumen produced supply costs (right, red), while mined bitumen supply costs are increasing after 2020 (left, red), driven by resource exhaustion.

The total costs (with carbon costs) show a similar pattern for mined bitumen, while total costs of in-situ produced bitumen are now increasing, driven by increasing carbon costs. This difference is explained by the fact that in-situ recovery techniques are much more carbon intensive than mining recovery techniques, hence the larger impact of carbon emissions when carbon costs are included.

#### b) Influences: Bitumen supply and total costs

The influences of each parameter on these results are examined more formally by using the regression sensitivity analysis in Palisade's @RISK. Mapped values show the change in costs in USD per barrel if one parameter increases by one standard deviation while all other parameters are constant (Palisade, 2008). Mapped values are the normalised regression coefficient associated with each input parameter, multiplied by the standard deviation of the output. The regressions mapped values are obtained from a simulation of 10,000 runs. These influences are shown for the years 2030 and 2050.

#### In-situ produced bitumen



Fig. 5: Regression mapped values - In-situ bitumen supply costs

The longer bars represent the most significant variables. Figure 5 shows the main regression mapped values for the years 2030, 2050 and 2070 in order to highlight the change in trend between 2050 and 2070. These results are discussed below.

The results show that the initial cost has the biggest influence on supply costs in 2030. The learning rate is the second most influential parameter in 2030. The sign of the sensitivity associated with the learning rate parameter is negative, as a higher learning rate will induce costs to decrease further. In 2080, the depletion exponent becomes the most influential parameter. As  $X_t/X_T \le 1$ , a higher exponent ( $\gamma$ ) means lower costs, hence the negative sign of the sensitivity. This shift in influence is revealed by a close examination of the influence of the production parameters  $x_{max}$  and  $t_1$ .

In 2030 and 2050, learning is the dominant effect and supply costs are decreasing, with learning being driven by production. The inflection time  $t_1$  is the time when the growth of the production rate starts to decline, therefore a smaller  $t_1$  means that production, and learning, happen sooner, hence the positive sign of the sensitivity. The same applies for the second production parameter  $x_{max}$  (maximum production rate). A higher maximum for the production rate means that more oil is produced, driving costs further down through learning.

Depletion, like learning, is driven by production. A smaller  $t_1$  means that production and depletion happen sooner, driving up supply costs in 2070 once depletion effects start to bite. The same applies to the maximum production rate

 $x_{max}$ . A higher value of the maximum production rate will increase supply costs in 2070.

The switch from learning to depletion being the dominant effect is shown by the change of sign of both influence between 2050 and 2070: negative to positive in the case of the maximum production rate  $x_{max}$ , and positive to negative in the case of the inflection time  $t_1$ .

 $X_T$  is the ultimately recoverable resources and only appears in the depletion term of the model. If the recovery factor R increases,  $X_T$  increases, postponing depletion and its upward effect on costs, hence the negative signs of the correlation sensitivities. The recovery factor R is more influential in 2070 than in 2050 while the sign of its sensitivity remains the same. This is explained by the fact that this parameter only appears in the depletion part of the model and that the depletion effect dominates over the learning effect in 2070.

#### Mined bitumen



Fig. 6: Regression mapped values - Mined bitumen supply costs

The results show that the depletion exponent and the maximum production rate have the biggest influence on supply costs in 2050. This time, the regression mapped values are shown for the years 2030, 2050 and 2010 in order to highlight the change in trend between 2010 and 2030. In 2010, learning is the dominant effect: supply costs are decreasing (mean and 5<sup>th</sup> percentile of the supply costs, in red on the left hand side of Figure 1), with learning being driven by production. The positive sign of the inflection time influence and the negative sign of the x<sub>max</sub> influence in 2010 show that learning is driving supply costs. However, this shift occurs earlier in the case of mined bitumen, as the ultimate volume of mineable bitumen is much smaller than the ultimate recoverable resources through in-situ techniques. With a similar production pattern to 2050, mining resources are depleted earlier than in-situ resources. Looking at these

influences will help us to identify the most influential parameters and refine the study by finding better estimates for these parameters.

## 4.2 Synthetic crude oil costs: with and without carbon costs

#### a) Synthetic crude oil costs over time

The results below show the supply (without carbon costs) and total costs (with carbon costs associated with bitumen production and upgrading) of Canadian synthetic crude oil over time.



Fig. 7: Costs of synthetic crude oil from mined bitumen, with and without carbon costs



# Fig. 8: Costs of synthetic crude oil from in-situ bitumen, with and without carbon costs

The results show the uncertainties on future costs of synthetic crude oil produced from mined and in-situ bitumen. Supply costs (without carbon) fall in the range of 28 to 63 USD per barrel in 2030 (2005 USD) for mined SCO, while insitu produced SCO supply costs fall in the range of 21 to 30 USD per barrel (2005 USD). In-situ costs show less uncertainty than mined SCO costs, as the former are mainly driven by learning parameters: learning dominates in the case of in-situ SCO supply costs (right, red), while mined SCO supply costs are increasing after 2020 (mean value, left, red), driven by the exhaustion of resources.

Comparing supply costs (in red) to total costs (in green) show the impact of carbon costs on the final costs of synthetic crude oil. As in the case of bitumen, carbon costs have a very large impact on the costs of producing synthetic crude oil from in-situ produced bitumen, more than doubling these costs in 2030 from 25 USD per barrel SCO to 58 USD per barrel SCO.

#### b) Influences: Synthetic crude oil supply and total costs

The influences of each parameter on these results are examined more formally by using the regression sensitivity analysis in Palisade's @RISK. Mapped values show the change in costs if one parameter changes by one standard deviation while all other parameters are constant, (Palisade, 2008). The regressions are obtained from a simulation of 10,000 runs.



Synthetic crude oil upgraded from in-situ bitumen





Fig. 10: Regressions mapped values - total costs of synthetic crude oil from insitu bitumen

The regression mapped values for the supply costs of in-situ synthetic crude oil (excluding carbon costs) show the same pattern as in the case of in-situ bitumen, with the addition of upgrading parameters. The most influential parameter in 2050 is the learning rate associated with upgrading bitumen into synthetic crude oil. In 2050, the depletion exponent becomes more influential than the learning rate associated with bitumen production in-situ. In the case of total costs (including carbon costs), the initial carbon cost parameter is the most influential parameters in 2050.

#### Synthetic crude oil upgraded from mined bitumen

Figures 11 and 12 show the regression mapped values associated with the supply costs (excluding carbon costs) and total costs (including carbon costs) of synthetic crude oil from mined bitumen.



Fig. 11: Regressions mapped values - supply costs of synthetic crude oil from mined bitumen



Fig. 12: Regressions mapped values - total costs of synthetic crude oil from mined bitumen

Again, the regression mapped values for the supply costs of synthetic crude oil show the same pattern as in the case of mined bitumen, with the addition of upgrading parameters. The most influential parameters in 2050 are still the depletion exponent and the maximum production rate.

In the case of total costs (including carbon costs), the depletion exponent parameter is still the most influential parameter in 2050. The second most influential parameter is the initial carbon cost. While in the case of synthetic crude oil from in-situ bitumen this parameter was of a higher order of magnitude than any other parameter, in the case of synthetic crude oil from mined bitumen the influence of the initial carbon costs is comparable to the influences of the maximum production rate, the depletion exponent and the mining recovery rate in 2050. So, while carbon costs have a significant effect on total costs of synthetic crude oil from mined bitumen, this effect is much smaller than in the case of synthetic crude oil from in-situ produced bitumen. Again, this is explained by the fact that in-situ recovery methods are much more carbon-intensive than mining recovery methods, and by the fact that the costs of mined bitumen are very much driven up by depletion.

# • 5. Conclusion

In this paper, a model describing the effects of learning, depletion and carbon emissions on the costs of supplying bitumen and synthetic crude oil from oil sands deposits has been introduced. The learning, depletion, production, resources and carbon parameters of the model are not known precisely, and uncertainty was introduced by assigning a distribution to each parameter: these uncertainties propagate through the model, resulting in large uncertainties for the future supply costs of synthetic crude oil.

The most influential parameters appear to be the learning parameters in the case of in-situ produced bitumen and the depletion parameters in the case of mined bitumen. Carbon costs have a large impact of the total costs of synthetic crude oil, in particular in the case of synthetic crude oil from in-situ bitumen, due to the carbon-intensity of the recovery techniques: taking into account the social cost of carbon adds more than half to the cost of producing synthetic crude oil from mined bitumen in 2050 (mean value), while the cost of producing synthetic crude oil from in-situ bitumen is multiplied by three. The results show that the social cost of carbon has a significant impact on the marginal cost of synthetic crude oil from Canadian oil sands. This effect could have a large impact on the price of oil when synthetic crude oil becomes the marginal source of crude oil supply.

The potential impact of additional liquid fuel production, including synthetic crude oil and first generation biofuels, on the world oil market and world oil prices will be assessed in future research. The political, social and economic acceptability of a tax on fuels from non-conventional oil and biofuels will also be studied. Finally, the study will explore the consequences of the above on the development of international investments and markets for biofuels and non-conventional oil.

## References

Adelman, M.A., 2004. The Real Oil Problem. *Regulation*. 27 (1) 16-21 Available from: http://web.mit.edu/ceepr/www/R2004-171.pdf

Adelman, M. A., 1993. Mineral Scarcity and Depletion: Theory and Measurement, in *The Economics of Petroleum Supply*, MIT Press Cambridge, MA.

Alberta Chamber of Resources, 2004. Oil sands technology roadmap – Unlocking the potential.

Available from: http://www.acr-alberta.com

Alberta Energy and Utilities Board (AEUB), 2006. Alberta's Energy Reserves 2005 and Supply/Demand Outlook 2006-2015. Alberta Energy and Utilities Board, Calgary, Alberta.

Alberta Energy and Utilities Board (AEUB), 2003. Alberta's Reserves 2003 and Supply/Demand Outlook 2004-2013. Alberta Energy and Utilities Board, Calgary, Alberta.

Alpert, W., Raiffa, H. (1969) A progress report on the training of probability assessors. Unpublished manuscript, 1969, (1, 22, 33)

Anderson, D., Winne, S., 2003. Innovation and Threshold Effects in Technology Responses to Climate Change. Tyndall Centre for Climate Change Research Available from: http://www.tyndall.ac.uk/publications/working\_papers/wp43.pdf

Attanasi, E.D., 1995. Economics and the 1995 National Assessment of United States Oil and Gas Resource. US Geological Survey (USGS). United States Geological Survey Circular 1145

Available from: http://pubs.usgs.gov/circ/1998/c1145/c114.pdf

Browne, J., 2006. Energy Security and Climate Change – Speech of BP CEO to Columbia Business School, New York, U.S.A. Available from: http://www.bp.com/genericarticle.do?categoryId=98&contentId=7025859

http://www.bp.com/genericarticle.do?categoryId=98&contentId=7025859

Canadian Association of Petroleum Producers (CAPP), 2006. Canadian Crude oil production and supply forecast 2006 – 2020. Available from: http://www.capp.ca/raw.asp?x=1&dt=NTV&e=PDF&dn=103586

Canadian Association of Petroleum Producers (CAPP), 2009. Statistical Handbook, Canadian synthetic and bitumen production. Available from: http://www.capp.ca

Canadian Association of Petroleum Producers (CAPP), 2007. 2007 CAPP Stewardship report – Facing our challenges.

Available from: http://stewardship.capp.ca/Environment/greenhouse\_gass.html

Canadian Association of Petroleum Producers (CAPP), 2004. A National Inventory of Greenhouse Gas (GHG), Criteria Air Contaminant (CAC) and Hydrogen Sulphide (H2S) Emissions by the Upstream Oil and Gas Industry, Technical report, Volume 1, Overview of the GHG Emissions Inventory Available from: http://www.capp.ca/raw.asp?x=1&dt=NTV&e=PDF&dn=86220

Canadian Energy Research Institute (CERI), 2005. Economic Impacts of Alberta's Oil Sands Volume 1 Available from: http://www.ceri.ca/Publications/documents/OilSandsReport-Final.PDF

Chakravorty, U., 1997. Endogenous substitution among Energy Resources and Global Warming. *The Journal of Political Economy* 

Chakravorty, U., Roumasset, J., 1990. Competitive oil prices and scarcity rents when the extraction cost function is convex. *Resources and Energy*. 12, 311-320.

Chevron, 2009. Climate change. http://www.chevron.com/globalissues/climatechange/

Cliffe, K., 2002. Oil Sands Working Paper, Petroleum Resources Division, Natural Resources Canada, unpublished manuscript, May 14.

Cupcic, F., 2003. Recovery Factor - The Challenges of Enhanced Recovery Available from: http://www.peakoil.net/iwood2003/ppt/CupcicPresentation.pdf

de Finetti, B. 1968 Probability: Interpretations. In D.E.Sills (Ed.), International Encyclopedia of the Social Sciences (Vol 12). New York: MacMillan , 1968, pp 496-504

Emerson, M. 1988. The economics of 1992. Oxford University Press.

Energy Information Administration (EIA) 2009a. World Oil balance 2005-2008. June 2009 International Petroleum Monthly, posted on July 7, 2009.

Energy Information Administration (EIA) 2009b. Energy Information Administration / International Energy Outlook 2009 – Chapter 2 : World Liquid Fuels Analysis to 2030 http://www.eia.doe.gov/oiaf/ieo/pdf/liquid fuels.pdf

Energy Information Administration (EIA), 2009c. International Petroleum Monthly (IPM) World annual petroleum (Oil) production 1977 - 2005. Available from: www.eia.doe.gov/ipm/supply.html

Energy Information Administration (EIA), 2009d. International energy statistics - Refining capacity

Available from: http://tonto.eia.doe.gov/cfapps/ipdbproject/iedindex3.cfm

Energy Information Administration (EIA), 2007a. Performance Profiles of Major Energy Producers 2007 Available from: http://www.eia.doe.gov/emeu/perfpro/t&f\_o&g.html

Energy Information Administration (EIA), 2007b. Refining and Marketing Available from: http://www.eia.doe.gov/emeu/perfpro/r&m.pdf

Energy Information Administration (EIA), 2003. The Impact of Environmental Compliance Costs on U.S. Refining Profitability, 1995 - 2001 http://www.eia.doe.gov/emeu/perfpro/ref\_pi2/refpi2.pdf

Energy Resources Conservation Board (ERCB, formerly AEUB), 2008. Alberta's Energy Reserves 2008 and Supply/Demand Outlook 2009-2018

Environment Canada, 2008. Canada's greenhouse gas emissions – Understanding the trends

http://www.ec.gc.ca/pdb/ghg/inventory\_report/2008\_trends/trends\_eng.cfm#t oc\_2\_1

ExxonMobil, 2009. Reducing greenhouse gas emissions from energy production http://www.exxonmobil.com/Corporate/images/enlarged\_ghg\_combo.gif

Farrell, A. E., Brandt, A. R., 2006. Risks of the oil transition *Environ. Res. Lett.* 1 (2006) 014004 (6pp)

Flint, L. 2004. Bitumen and very heavy crude upgrading technology - a review of long term r&d opportunities. LENEF Consulting (1994) Limited http://www.ptac.org/links/dl/osdfnlreport.pdf

Grand Dictionnaire Terminologique, 2007. Definitions Available from: http://www.granddictionnaire.com/

Greene, D. L., Hopson, J. L., Li, J., 2005. Have we run out of oil yet? Oil peaking analysis from an optimist's perspective. *Energy Policy.* 34 (5), 515-531

Grubb, M., 2001. Who's afraid of atmospheric stabilization? Making the link between energy resources and climate change. *Energy policy*. 29, 837-845.

Grübler, A., Nakicenovic, N., Victor, D.G., 1999. Dynamics of energy technologies and global change. *Energy Policy*. 27, 247–280.

Hartwick, J. M., 1978. Exploitation of many deposits of an exhaustible resource, *Econometrica*. 46 (1)

Hope, C., 2008. The impacts of Climate Change: what do we know, how do we know it, and what should we do? Presentation prepared for CUEN.

Hope, C., 2007. The social cost of carbon. Presentation prepared for the JETRO – Clare Hall – CEI Seminar on Energy, Environment and Climate Change. Available from: http://www.jetro.go.jp

Hope, C., 2006. The marginal impact of CO2 from PAGE2002: An integrated assessment model incorporating the IPCC's five reasons for concern. *Integrated Assessment*. 6 (1) 19-56

Hotelling, H., 1931. The Economics of Exhaustible Resources. *The Journal of Political Economy*. 39 (2) 137-175

Huntington, H.G., 1993. OECD oil demand - Estimated response surfaces for nine world oil models. Energy Economics

International Energy Agency (IEA), 2007. Statement on the Current Oil Market Situation Available from: http://www.iea.org

International Energy Agency (IEA), 2005a. Resources to reserves. OECD/IEA, Paris

International Energy Agency (IEA), 2005. The European refinery industry under the EU emissions trading scheme - Competitiveness, trade flows and investment implications, IEA Paris.

International Energy Agency (IEA), 2002. Background Paper on IEA Conference on Prospects for Non-Conventional Oil, Calgary Canada, November 25-26, 2002, IEA Paris.

International Energy Agency (IEA), 2000. *Experience curves for energy technology policy*, by Wene, C.O. OECD/IEA, Paris

Junius, K., 1997. Economies of Scale: A Survey of the Empirical Literature. Kiel working paper No 813.

Available from: http://papers.ssrn.com/sol3/papers.cfm?abstract\_id=8713

Kahouli-Brahmi, S. 2008. Technological learning in energy-environmenteconomy modelling: a survey. Energy Policy 36 (1) 138-162

Köhler, J., Grubb, M., Popp, D., Edenhofer, O., 2006. The Transition to Endogenous Technical Change in Climate-Economy Models: A Technical Overview to the Innovation Modeling Comparison Project. *The Energy Journal*, Endogenous Technological Change and the Economics of Atmospheric Stabilisation Special Issue

Krautkraemer, J., Toman, M., 2003. Fundamental Economics of Depletable Energy Supply. Resources for the Future. Discussion Paper 03-01 Available from: http://www.rff.org/documents/RFF-DP-03-01.pdf Lieberman, M.B., 1984. The learning curve and pricing in the chemical processing industries, Rand Journal of Economics 15, 213–228

Lindley, D. V., 1985. *Making decisions*, Second edition. John Wiley and sons, London.

NRCan, 2003. North American Issues Arising from the 2050, Study Transportation Research Board Conference - Washington, DC, presented by Paul Khanna Available from:

http://cta.ornl.gov/trbenergy/trb\_documents/khanna\_NA\_issues.pdf

Nordhaus, W., Boyer, J., 1999. Roll the DICE Again: Economic Models of Global Warming - Chapter 3

Margolis, R. M., 2002. Experience Curves and Photovoltaic technology policy, Human Dimensions of Global Change Seminar, Carnegie Mellon University. Available from: http://hdgc.epp.cmu.edu/mailinglists/hdgcctml/mail/ppt00010.ppt

McDonald, A., Schrattenholzer, L., 2001. Learning rates for energy technologies. *Energy Policy*. 29 (4) 255-261

Méjean, A., Hope, C., 2008. Modelling the costs of non-conventional oil: A case study of Canadian Bitumen. Energy Policy 36 (11)

National Energy Board (NEB), 2006. Canada's Oil Sands - Opportunities and Challenges to 2015: An Update. Available from: http://www.neb.gc.ca

National Energy Board (NEB), 2004. Canada's Oil Sands - Opportunities and Challenges to 2015. Available from: http://www.neb.gc.ca

National Energy Board (NEB), 2000. Canada's Oil Sands: A Supply and Market Outlook to 2015. Available from: http://www.neb.gc.ca

Nehring, R., 1982. Prospects for conventional world oil resources. Annu. Rev. Energy 7:175–200

Nordhaus, W., Boyer, J., 1999. Roll the DICE Again: Economic Models of Global Warming - Chapter 3 Available from:

http://www.econ.yale.edu/~nordhaus/homepage/web\%20chap\%203\%201 02599.pdf

Odell, P., 1998. Dynamics of energy technologies and global change. *Energy policy*. 27, 737-742.

Palisade, 2008. @Risk 5 Help.

Rogner, H-H., 1997. An Assessment of World Hydrocarbon Resources. *Annual Review Energy Environment* 22, 217-62.

Roumasset, J., Isaak, D., Fesharaki, F., 1983. Oil prices without OPEC A walk on the supply-side. *Energy Economics*. 5 (3) 164-170 Available from: http://www.sciencedirect.com

SAUNER, 2000a. The SAUNER project: Summary final report

SAUNER, 2000b. Technical data summary: Oil. Cost of conventional oil. Available from: http://people.bath.ac.uk/hssam/sauner/mainresults.html

Savage, L. J. 1954 The foundations of statistics. New York: Wiley (1, 25).

Soderbergh, B., 2006. A crash programme scenario for the Canadian oil sands industry. *Energy policy*. In press.

Staël von Holstein, C.-A. S. (1971b) Two techniques for assessment of subjective probability distributions – An experimental study. Acta Psychologica , 1971, 35, 478-494.

Stern, N., 2007. *The Economics of Climate Change - The Stern Review*. Cambridge University Press. Cambridge, U.K.

Sweeney, J., L., 1992. Economic theory of depletable resources: An Introduction, in

*Handbook of Natural Resource and Energy Economics,* Volume 3. Eds. Allen V. Kneese and James L. Sweeney.

Toman, M., Curtright, A.E., Ortiz, D.S., Darmstadter, J., Shannon, B., 2008. Unconventional Fossil-Based Fuels Economic and Environmental Trade-Offs. RAND Technical Report.

Tsuchiya, H., Kobayashi, O., 2003. Mass production cost of PEM fuel cell by learning curve. *International Journal of Hydrogen Energy*. 29, 985-990.

Tversky, A. and Kahneman, D. (1974) Judgement under uncertainy: Heuristics and biases. In Kahneman, D., Slovic, P. and Tversky, A. (Eds), Judgement under uncertainy: Heuristics and biases. Cambridge: Cambridge University Press, 1982, pp 3-20.

U.S. Geological Survey (USGS), 2005. Geology and Resources of Some World Oil-Shale Deposits, by John R. Dyni. Available from: http://pubs.usgs.gov/sir/2005/5294/ U.S. Geological Survey (USGS), 2003. Heavy Oil and Natural Bitumen – Strategic Petroleum Resources, by Meyer, R. F. and Attanasi, E. D., United States Geological Survey Fact Sheet 70-03

Available from: http://pubs.usgs.gov/fs/fs070-03/fs070-03.html

U.S. Geological Survey (USGS), 1989. An assessment of coal resources available for development, Central Appalachian region, Chapter 8 - Glossary, by M. Devereux Carter and Nancy K. Gardner. U.S. Geological Survey Open-File Report 89-362

Available from: http://pubs.usgs.gov/of/1989/of89-362/glossary.htm

Web dictionary of Cybernetics and Systems, 2007. Decision Theory Available from: http://pespmc1.vub.ac.be/ASC/indexASC.html Alberta Chamber of resources, 2004. Oil sands technology roadmap – Unlocking the potential.

Winkler, R. L. 1967 The assessment of prior distributions in Bayesian analysis . Journal of the American Statistical association, 1967, 62, 776-800.

# • Appendix: CO<sub>2</sub> emissions

Process	Unit (GHG)	2001	2002	2003	2004	2005	2006
Conventional oil and gas	ton/m3 oe	0.28	0.25	0.22	0.24	0.23	0.24
	ton/boe	0,034	0,030	0,026	0,029	0,028	0,029
In-situ	ton/m3 oe	0.68	0.51	0.49	0.48	0.45	0.45
	ton/boe	0,082	0,061	0,059	0,058	0,054	0,054
Mined and ungraded	ton/m3 oe		0.6	0.58	0.53	0.5	0.48
Milleu allu upgradeu	ton/boe		0,072	0,070	0,064	0,060	0,058

Source: (CAPP, 2007 p41)

Table A.1: Process emissions, 2001-2006 (CAPP, 2007)

Emissions (tCO2eq/barrel SCO)	In-situ (SAGD) + upgrading		Mining + upg	rading
Process	Natural gas	Residue	Natural gas	Residue
Recovery energy	0.05	0.085	0.012	0.024
Purchased power + miscellaneous	0.01	0.01	0.021	0.021
Upgrader net energy	0.01	0.015	0.01	0.015
Purchased power	0.005	0.005	0.005	0.005
H2 for 34 API SCO	0.025	0.04	0.025	0.04
Added H2 for 40 API SCO	-	0.02	-	0.02
Miscellaneous	0.005	0.005	0.005	0.005
Total	0.105	0.180	0.088	0.130
Total recovery only	0.06	0.095	0.033	0.045
Total recovery only (tCO <sub>2eq</sub> /barrel bitumen)	0.049-0.054	0.077-0.086	0.027-0.030	0.037-0.041
Total upgrading only	0.045	0.085	0.045	0.085

Adapted from: (Flint, 2004 p20)

 Table A.2: Process emissions (Flint, 2004)